

Error Analysis in an Iterative Algorithm for the Solution of the Regulator Equations for Distributed Parameter Systems

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Outline

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- 2 β -Iterative Scheme
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Statement of Problem

- Consider a MIMO plant modeled by a linear system

$$z_t(t) = Az(t) + B_{in}u(t) + B_d d(t),$$

$$z(0) = z_0,$$

$$y(t) = Cz(t).$$

We are given

- y_r a signal to be tracked,
 - d a disturbance to be rejected.
- $z(t)$ is the state variable in the infinite dimensional Hilbert space \mathcal{Z} .
 - Problem:
Find the time dependent controller $u(t)$ such that $y = Cz(t)$ satisfies

$$\lim_{t \rightarrow \infty} \|y_r(t) - y(t)\| = 0.$$

Statement of Problem Cont'd.

- A is an unbounded sectorial operator with dense domain $\mathcal{D}(A)$.
- A generates an exponentially stable analytic semigroup e^{At} in \mathcal{Z}

$$\|e^{At}\| < Me^{-at} \quad a > 0 \text{ and } M > 1.$$

- $B_{\text{in}} \in \mathcal{L}(\mathbb{R}^k, \mathcal{Z})$, and $B_d \in \mathcal{L}(\mathbb{R}^m, \mathcal{Z})$.
- C is unbounded but is relatively bounded by a fractional power of $(-A)$. There exists $s \in (0, 2)$ s.t.

$$C \in \mathcal{L}(\mathcal{H}^s, \mathbb{R}^k), \quad \text{where } \mathcal{H}^s = \mathcal{D}((-A)^{s/2}).$$

- Without loss of generality, by rescaling, we assume

$$-CA^{-1}B_{\text{in}} = I.$$

Dynamic Controller (DC)

- DC

For given $y_r(t)$ and $d(t)$

find \bar{z} , $\bar{\gamma}(t)$ and \bar{z}_0 satisfying

$$\dot{\bar{z}}_t = A\bar{z} + B_{in}\bar{\gamma}(t) + B_d d(t),$$

$$\bar{z}(0) = \bar{z}_0,$$

such that

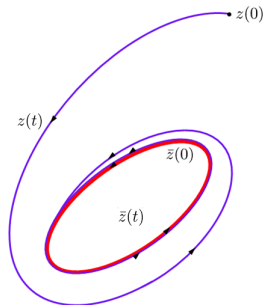
$$C\bar{z}(t) = y_r(t), \quad \forall t \geq 0.$$

- In the closed loop system, we set

$u(t) = \bar{\gamma}(t)$, and expect

$$\lim_{t \rightarrow \infty} \|Cz(t) - C\bar{z}(t)\| = 0,$$

for any initial data z_0 .



Why the Dynamic Controller?

- In the classical geometric method $y_r(t)$ and $d(t)$ are generated by a finite dimensional exogenous system (exosystem)
- In this case we obtain a system of two functional equations called the Regulation Equations
- Solvability of the Regulator Problem is equivalent to the solvability of the Regulator Equations
- Solving the Regulator Equations is not easy.
- The Exosystem might be non-linear.
- The Exosystem might be infinite dimensional.
- The plant could be non-linear.

Regularized Dynamic Controller RDC

- We can rewrite the DC as

$$(I + B_{in}CA^{-1})\bar{z}_t = A\bar{z}(t) + B_{in}y_r(t) + (I + B_{in}CA^{-1})B_d d(t).$$

- For $0 < \beta < 1$ we set,

$$(I + (1-\beta)B_{in}CA^{-1})\bar{z}_t^1 = A\bar{z}^1(t) + B_{in}y_r(t) + (I + B_{in}CA^{-1})B_d d(t).$$

Regularized Dynamic Controller RDC, The Equivalent Form

$$\bar{z}_t^1 = A_\beta \bar{z}^1(t) + \frac{1}{\beta} B_{in} y_r(t) + F d(t),$$

where $A_\beta = \left(A - \frac{(1-\beta)}{\beta} B_{in} C \right)$, $F = (I + B_{in} CA^{-1}) B_d$.

The control can be a posteriori evaluated as

$$\bar{\gamma}^1(t) = y_r(t) - (1 - \beta) CA^{-1}(\bar{z}_t^1) + CA^{-1} B_d d(t).$$

Corollary (Lassi Paunonen)

For $\delta = \frac{1-\beta}{\beta}$ sufficiently close to 0 (thus for β sufficiently close to 1) $A_\beta = A - \delta B_{in} C$ generates an exponentially stable semigroup.

General Form of RDC

- We solve the following RDC in each iteration $i = 1, 2, \dots$, for given target $y_r(t)$ and disturbance $\mathcal{D}(t)$.

$$\bar{z}_t^i = A_\beta \bar{z}^i(t) + \frac{1}{\beta} B_{\text{in}} y_r(t) + F \mathcal{D}(t).$$

- Then $\bar{\gamma}^i(t)$ can be written in following explicit form.

$$\bar{\gamma}^i(t) = y_r(t) - (1 - \beta) C A^{-1}(\bar{z}_t^i) + C A^{-1} B_{\text{in}} \mathcal{D}(t).$$

β -iterative scheme

Find approximate values for $\bar{z}(t)$ and $\bar{\gamma}(t)$ by seeking

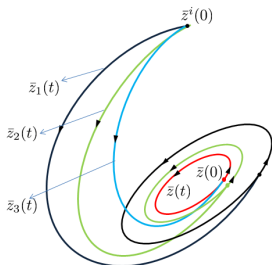
$$\bar{z}_n(t) = \sum_{j=1}^n \bar{z}^j(t), \quad \bar{\gamma}_n(t) = \sum_{j=1}^n \bar{\gamma}^j(t)$$

with $\bar{z}_n(t) \xrightarrow{n \rightarrow \infty} \bar{z}(t)$ and $\bar{\gamma}_n(t) \xrightarrow{n \rightarrow \infty} \bar{\gamma}(t)$.

$$E_1(t) = y_r(t) - C(\bar{z}^1(t)),$$

and for $i = 2, 3, \dots, n$,

$$E_i(t) = E_{i-1}(t) - C(\bar{z}^i(t)).$$



β -Iterative Algorithm

- Iteration 0: Solve Set Point control problem for $\bar{z}^0(x)$ for tracking $y_r(0)$ and rejecting $d(0)$.
- Iteration 1: Solve RDC for $\bar{z}^1(x)$ by setting $\mathcal{Y}_r(t) = y_r(t)$ and $\mathcal{D}(t) = d(t)$ with the I.C. $\bar{z}^1(x, 0) = \bar{z}^0(x)$.
- Iteration $i > 1$: Solve RDC for $\bar{z}^i(x)$ by setting $\mathcal{Y}_r(t) = E_{i-1}(t)$ and $\mathcal{D}(t) = 0$ with the I.C. $\bar{z}^i(x, 0) = 0$.

Error as a convolution integral.

Let us define

$$K(t) = -CA_{\beta}^{-1}e^{A_{\beta}t}\frac{1}{\beta}B_{\text{in}} \text{ and}$$

$$K_d(t) = -CA_{\beta}^{-1}e^{A_{\beta}t}(I + B_{\text{in}}CA^{-1})B_d,$$

- It can be shown that the first iteration error is given by

$$E_1(t) = y_r(t) - C(\bar{z}^1(t)) = K * y_r'(t) + K_d * d'(t).$$

- and the error at the i th-iteration is given by

$$E_i(t) = E_{i-1}(t) - C(\bar{z}^i) = K * E'_{i-1}(t) \text{ for } i = 2, \dots, n.$$

Theorem

Assume $y_r, d \in C_b^n[0, \infty)$ and let β_0 s.t. A_β generates an exponentially stable analytic semigroup in \mathcal{Z} for $\beta \in (\beta_0, 1)$. Then for any $T \geq 0$ we have

$$E_n(t) = \mathcal{E}_{1,T,n}(t) + \mathcal{E}_{2,T,n}(t)$$

where $\limsup_{t \rightarrow \infty} |\mathcal{E}_{1,T,n}(t)| = 0$ and

$$\begin{aligned} & \sup_{t \in [T, \infty)} |\mathcal{E}_{2,T,n}(t)| \\ & \leq D^n \left(\sup_{t \in [T, \infty)} |y_r^{(n)}(t)| + \beta \|B_{in}\|^{-1} \|B_d\| \sup_{t \in [T, \infty)} |d^{(n)}(t)| \right), \end{aligned}$$

where $D(A, B_{in}, C, \beta)$ is a constant.

Example 1: 1D Heat Equation with no disturbance

- We consider the control system defined on $0 \leq x \leq 1$ for $t \geq 0$ given by

$$\frac{\partial z(t)}{\partial t} = Az(t) + B_{\text{in}}u(t),$$

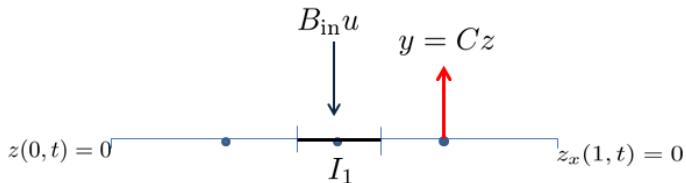
$$z(0, t) = 0, \frac{\partial z}{\partial x}(1, t) = 0,$$

$$z(x, 0) = 0,$$

$$y(t) = Cz(t), y_r(t) = \cos(t).$$

- In this case we define the operator $A = \frac{d^2}{dx^2}$ with domain $\mathcal{D}(A) = \{\varphi \in H^2(0, 1) : \varphi(0) = 0, \varphi'(1) = 0\}$ in the Hilbert state space $\mathcal{Z} = L^2(0, 1)$.

- $Cz(t) = z(0.75, t)$.
- $B_{\text{in}}u(t) = \frac{1}{|I_1|}\chi_{I_1}u(t)$.
- $I_1 = (0.5 - \delta, 0.5 + \delta)$.



- We set $\delta = 0.05$.

Continuous dependence with respect to β for the eigenvalues of

$$A_\beta = A - \frac{1 - \beta}{\beta} B_{in} C$$

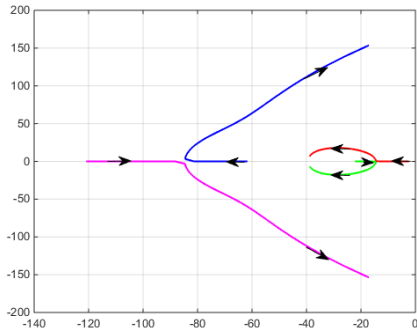


Figure 1 : Eigenvalues λ_1 , λ_2 , λ_3 , and λ_4 for β varying from 1 to 0.01.

For $\beta = 0.27$, the plot of e_1 (green), e_2 (blue) and e_3 (red).

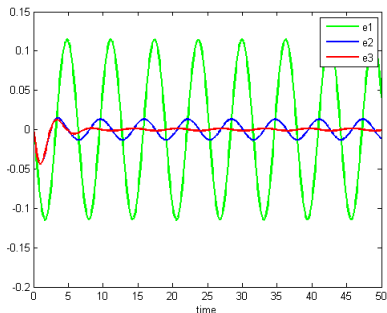


Figure 2 : The first three iteration errors.

$$D \sim 0.1$$

$0 \leq t \leq 20$	Error
$\ e_1\ _\infty$	1.15×10^{-1}
$\ e_2\ _\infty$	4.37×10^{-2}
$\ e_3\ _\infty$	4.36×10^{-2}
$20 \leq t \leq 35$	Error
$\ e_1\ _\infty$	1.15×10^{-1}
$\ e_2\ _\infty$	1.32×10^{-2}
$\ e_3\ _\infty$	1.52×10^{-3}
$35 \leq t \leq 50$	Error
$\ e_1\ _\infty$	1.15×10^{-1}
$\ e_2\ _\infty$	1.32×10^{-2}
$\ e_3\ _\infty$	1.52×10^{-3}

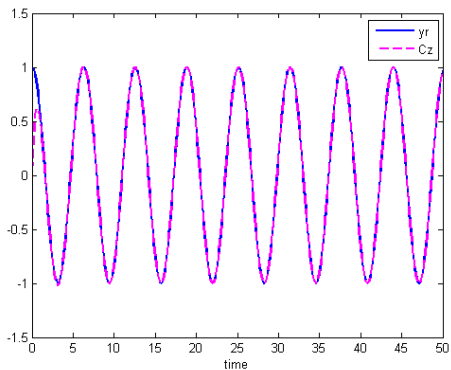


Figure 3 : y_r and $C(z)$.

Example 2: 1D Heat Equation with nonlinear Exosystem

We consider the control system defined on $0 \leq x \leq 1$ for $t \geq 0$ given by

$$\frac{\partial z(t)}{\partial t} = Az(t) + B_{\text{in}}u(t) + B_{\text{d}}d(t),$$

$$z(0, t) = 0, \quad \frac{\partial z}{\partial x}(1, t) = 0,$$

$$z(x, 0) = 0,$$

$$y(t) = Cz(t) = z(1, t).$$

In this case we define the operator $A = \frac{d^2}{dx^2}$ with domain

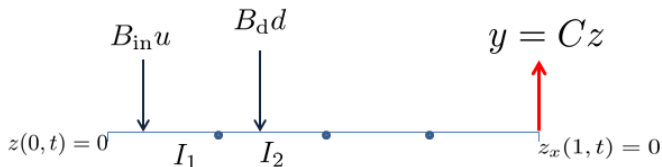
$$\mathcal{D}(A) = \{\varphi \in H^2(0, 1) : \varphi(0) = 0, \quad \varphi'(1) = 0\}$$

in the Hilbert state space $\mathcal{Z} = L^2(0, 1)$.

In our specific numerical example we have set

$$I_1 = \{x : 0 \leq x < 1/4\},$$

$$I_2 = \{x : 1/4 \leq x \leq 1/2\},$$



The reference signal y_r and the disturbance d are given by the solution of

$$\ddot{\omega} + \dot{\omega} - \omega + \omega^3 = 0,$$

s.t

for the I.C $\omega(0) = 0, \dot{\omega}(0) = 1.7, \quad y_r(t) = \omega(t) \rightarrow 1$ as $t \rightarrow \infty$,

for the I.C $\omega(0) = 1, \dot{\omega}(0) = 1, \quad d(t) = \omega(t), \rightarrow -1$ as $t \rightarrow \infty$.

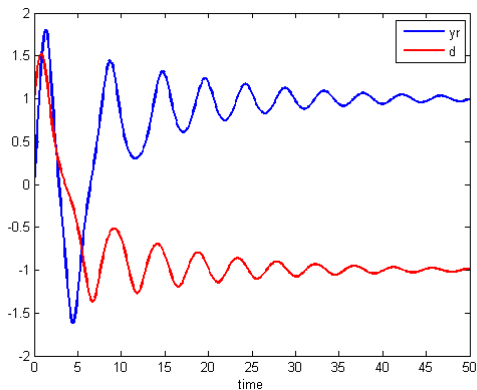


Figure 4 : The reference y_r and disturbance d .

For $\beta = 0.1$, the plot of e_1 (green), e_2 (blue) and e_3 (red).

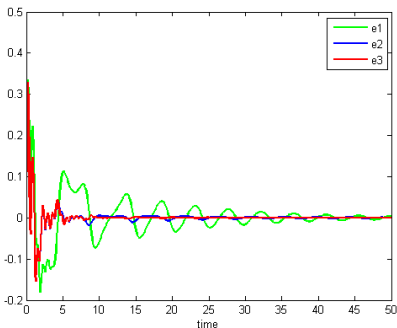


Figure 5 : The first three iteration errors.

$$D \sim 0.14$$

$0 \leq t \leq 20$	Error
$\ e_1\ _\infty$	3.36×10^{-1}
$\ e_2\ _\infty$	3.29×10^{-1}
$\ e_3\ _\infty$	3.29×10^{-1}
$20 \leq t \leq 35$	Error
$\ e_1\ _\infty$	3.43×10^{-2}
$\ e_2\ _\infty$	4.67×10^{-3}
$\ e_3\ _\infty$	1.18×10^{-3}
$35 \leq t \leq 50$	Error
$\ e_1\ _\infty$	1.06×10^{-2}
$\ e_2\ _\infty$	1.53×10^{-3}
$\ e_3\ _\infty$	2.22×10^{-4}

For $\beta = 0.1$

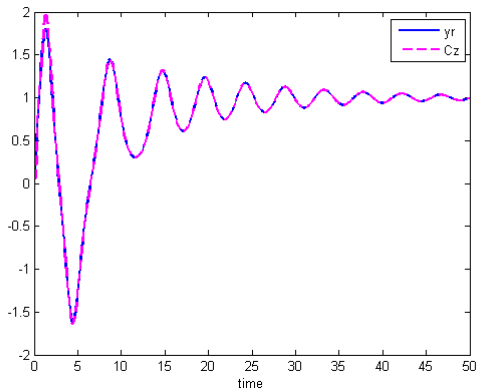


Figure 6 : y_r and $C(z)$

Example 3: Thermal regulation of a Navier-Stokes Flow

$$\rho(\mathbf{v} \cdot \nabla)\mathbf{v} - \nabla \cdot \left[\mu(\nabla\mathbf{v} + (\nabla\mathbf{v})^T) \right] + \nabla p = 0, \quad \nabla \cdot \mathbf{v} = 0,$$

$$\frac{\partial T}{\partial t} = \alpha \Delta T - \mathbf{v} \cdot \nabla T + B_{in}u + B_d d, \quad y(t) = CT(t),$$

$$y_r(t) = a + b \sin(\omega_1 t), \quad d(t) = c + d \sin(\omega_2 t)$$

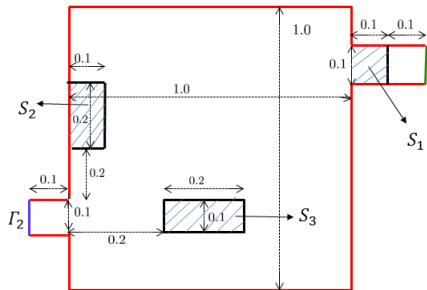
$$\mathbf{v}(x, 0) = 0, p(x, 0) = 0, T(x, 0) = 0.$$

$$\mathbf{v} = 0 \text{ on } \Gamma_w,$$

$$\mathbf{v} = \begin{pmatrix} f(s) \\ 0 \end{pmatrix}, \quad T = 0 \text{ on } \Gamma_1,$$

$$-\alpha \nabla T \cdot \mathbf{n} = 0 \text{ on } \Gamma_2 \cup \Gamma_w,$$

$$\boldsymbol{\tau} = 0 \text{ on } \Gamma_2.$$



Here,

$$A = \alpha \Delta - \mathbf{v} \cdot \nabla, \quad \mathcal{D}(A) = \left\{ \varphi \in H^2(\Omega) : \varphi|_{\Gamma_1} = 0, -\alpha \nabla \varphi \cdot \mathbf{n}|_{\Gamma_2 \cup \Gamma_w} = 0 \right\}$$

in the Hilbert state space $\mathcal{Z} = L^2(\Omega)$.

$$CT(t) = \frac{1}{|S_3|} \int_{S_3} T ds,$$

$$B_{in} u(t) = \frac{1}{|S_1|} \chi_{S_1} u(t), \quad B_d d(t) = \frac{1}{|S_2|} \chi_{S_2} d(t).$$

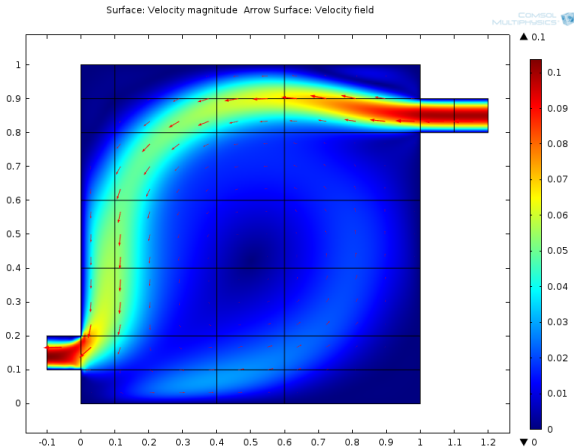


Figure 7 : The Velocity Profile.

For $\beta = 0.1$

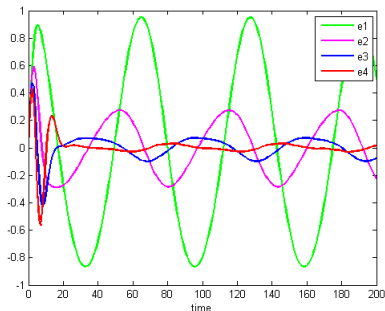


Figure 8 : The first three iteration errors.

$$D \sim 0.3$$

$0 \leq t \leq 100$	Error
$\ e_1\ _\infty$	9.51×10^{-1}
$\ e_2\ _\infty$	5.94×10^{-1}
$\ e_3\ _\infty$	4.72×10^{-1}
$\ e_4\ _\infty$	5.63×10^{-1}
$100 \leq t \leq 200$	Error
$\ e_1\ _\infty$	9.49×10^{-1}
$\ e_2\ _\infty$	2.86×10^{-1}
$\ e_3\ _\infty$	9.86×10^{-2}
$\ e_4\ _\infty$	3.10×10^{-2}

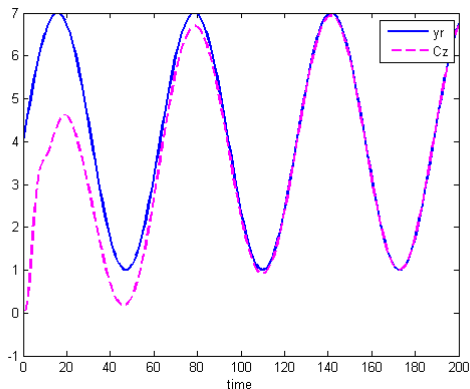


Figure 9 : y_r and the measured output of the closed loop system CT .

Future Work

- Obtain error estimates of the β -iterative method for control systems with
 - unbounded B
 - nonlinear state
- Build c++ PDE toolbox for solving Regulator Problem using the β -iterative method

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Thank You